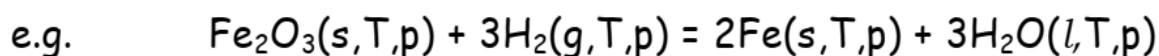


Thermochemistry

Much of thermochemistry is based on finding "easy" paths to calculate changes in enthalpy, i.e. understanding how to work with thermodynamic cycles.

- Goal: To predict ΔH for every reaction, even if it cannot be carried out in the laboratory

The heat of reaction ΔH_{rx} is the ΔH for the isothermal reaction at constant pressure (the complete transfer from reactants to products, not to some equilibrium state).



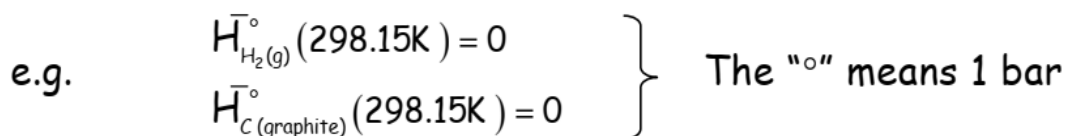
$$\Delta H_{rx}(T, p) = 2\bar{H}_{\text{Fe}}(T, p) + 3\bar{H}_{\text{H}_2\text{O}}(T, p) - 3\bar{H}_{\text{H}_2}(T, p) - \bar{H}_{\text{Fe}_2\text{O}_3}(T, p)$$

$$[\Delta H_{rx} = H(\text{products}) - H(\text{reactants})]$$

We cannot know \bar{H} values because enthalpy, like energy, is not an absolute scale. We can only measure differences in enthalpy.

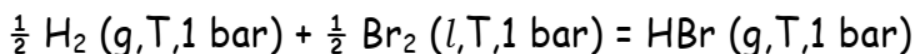
- Define a reference scale for enthalpy

$\bar{H}(298.15\text{K}, 1\text{ bar}) \equiv 0$ For every element in its most stable form at 1 bar and 298.15K



- $\Delta H_f^\circ(298.15\text{K})$: The heat of formation is the heat of reaction to create 1 mole of that compound from its constituent elements in their most stable forms.

Example ($T = 298.15\text{ K}$)

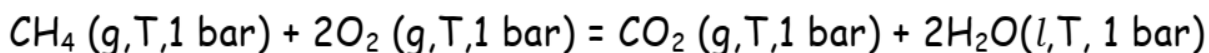


$$\Delta H_{f, \text{HBr}}^\circ(T) = \Delta H_{\text{rx}}(T, 1 \text{ bar}) = H_{\text{HBr}}^\circ(\text{g}, T) - \underbrace{\frac{1}{2} H_{\text{H}_2}^\circ(\text{g}, T) - \frac{1}{2} H_{\text{Br}_2}^\circ(\text{l}, T)}_{0 - \text{elements in most stable forms}}$$

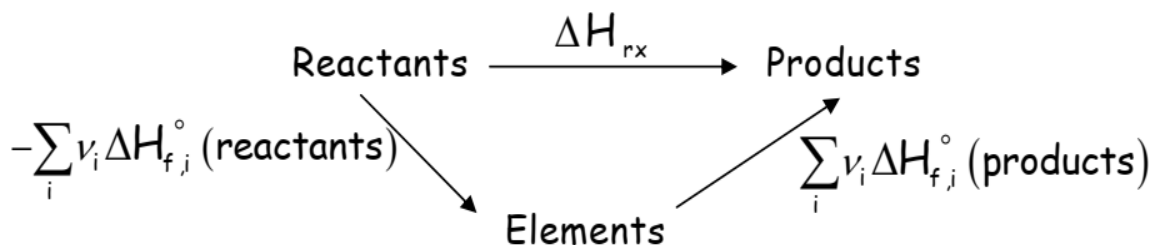
We can tabulate $\Delta H_f^\circ(298.15\text{K})$ values for all known compounds.

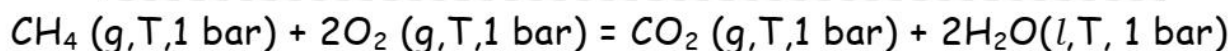
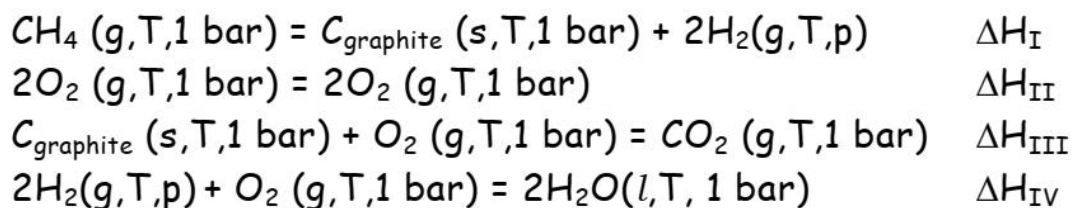
We can calculate $\Delta H_{\text{rx}}^\circ(298.15\text{K})$ for any reaction.

e.g. ($T=298.15\text{K}$)



- First decompose reactants into elements
- Second put elements together to form products
- Use Hess's law [An example of a thermodynamic cycle applied to thermochemistry]





$$\Delta H_{\text{rx}} = \Delta H_{\text{I}} + \Delta H_{\text{II}} + \Delta H_{\text{III}} + \Delta H_{\text{IV}}$$

$$\Delta H_{\text{I}} = \bar{H}_{\text{C}} + 2\bar{H}_{\text{H}_2} - \bar{H}_{\text{CH}_4} = -\Delta H_{\text{f}, \text{CH}_4}^{\circ}$$

$$\Delta H_{\text{II}} = \bar{H}_{\text{O}_2} - \bar{H}_{\text{O}_2} = 0$$

$$\Delta H_{\text{III}} = \bar{H}_{\text{CO}_2} - \bar{H}_{\text{C}} - \bar{H}_{\text{O}_2} = \Delta H_{\text{f}, \text{CO}_2}^{\circ}$$

$$\Delta H_{\text{IV}} = 2\bar{H}_{\text{H}_2\text{O}} - 2\bar{H}_{\text{H}_2} - \bar{H}_{\text{O}_2} = 2\Delta H_{\text{f}, \text{H}_2\text{O}}^{\circ}$$

$$\therefore \Delta H_{\text{rx}} = 2\Delta H_{\text{f}, \text{H}_2\text{O}}^{\circ} + \Delta H_{\text{f}, \text{CO}_2}^{\circ} - \Delta H_{\text{f}, \text{CH}_4}^{\circ}$$

In general,

$$\Delta H_{\text{rx}} = \sum_i \nu_i \Delta H_{\text{f}, i}^{\circ} (\text{products}) - \sum_i \nu_i \Delta H_{\text{f}, i}^{\circ} (\text{reactants})$$

$\nu \equiv$ stoichiometric coefficient

- ΔH at constant p and for reversible pV process is $\Delta H = q_p$

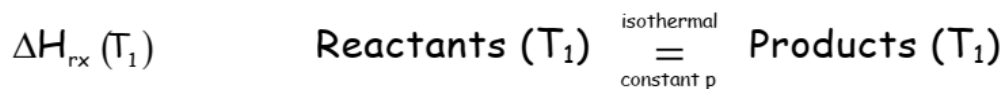
\Rightarrow The heat of reaction is the heat flowing into the reaction from the surroundings

If $\Delta H_{\text{rx}} < 0$, $q_p < 0$ heat flows from the reaction to the surroundings (exothermic)

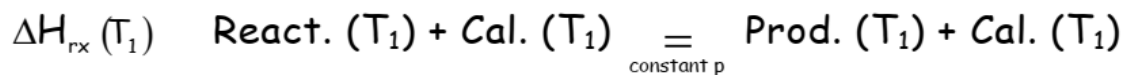
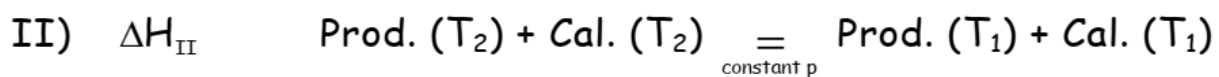
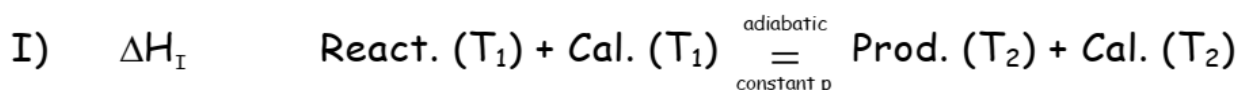
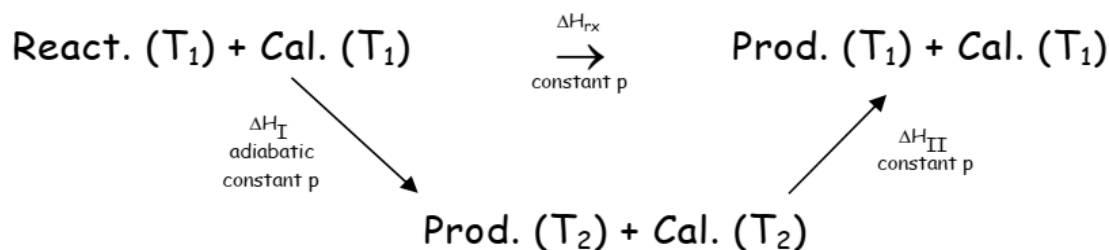
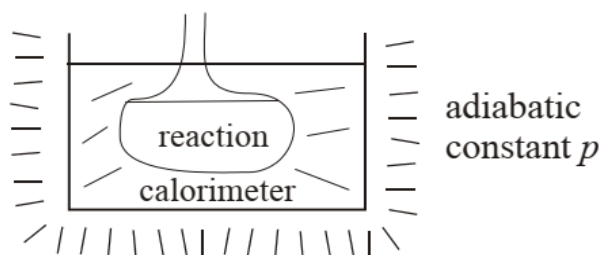
If $\Delta H_{\text{rx}} > 0$, $q_p > 0$ heat flows into the reaction from the surroundings (endothermic)

Calorimetry

The objective is to measure



- Constant pressure (for solutions)



$$\Delta H_{rx}(T_1) = \Delta H_I + \Delta H_{II}$$

(I) Purpose is to measure $(T_2 - T_1)$

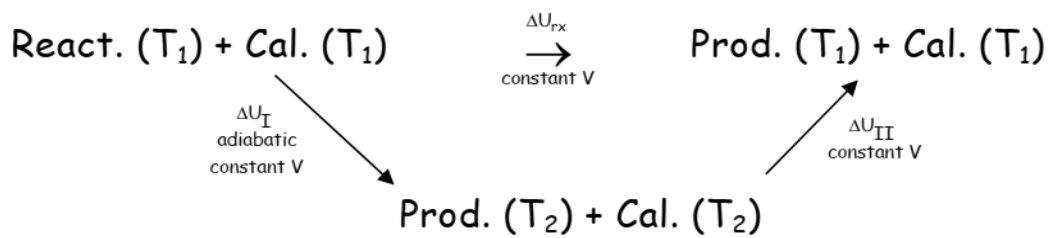
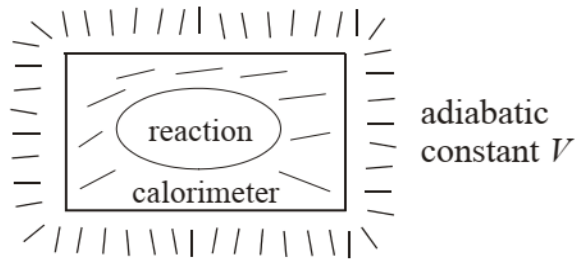
$$\text{Adiabatic, const. } p \Rightarrow q_p = 0 \Rightarrow \Delta H_I = 0$$

(II) Purpose is to measure heat q_p needed to take prod. + cal. from T_2 back to T_1 .

$$q_p = \int_{T_2}^{T_1} C_p (\text{Prod.} + \text{Cal.}) dT = \Delta H_{II}$$

$$\therefore \Delta H_{rx}(T_1) = - \int_{T_1}^{T_2} C_p (\text{Prod.} + \text{Cal.}) dT$$

- Constant volume (when gases involved)



$$\text{I) } \Delta U_I \quad \text{React. (} T_1 \text{) + Cal. (} T_1 \text{)} \stackrel{\text{adiabatic}}{=} \text{Prod. (} T_2 \text{) + Cal. (} T_2 \text{)}$$

$$\text{II) } \Delta U_{II} \quad \text{Prod. (} T_2 \text{) + Cal. (} T_2 \text{)} \stackrel{\text{constant } V}{=} \text{Prod. (} T_1 \text{) + Cal. (} T_1 \text{)}$$

$$\Delta U_{rx}(T_1) \quad \text{React. (} T_1 \text{) + Cal. (} T_1 \text{)} \stackrel{\text{constant } V}{=} \text{Prod. (} T_1 \text{) + Cal. (} T_1 \text{)}$$

$$\Delta U_{\text{rx}}(T_1) = \Delta U_{\text{I}} + \Delta U_{\text{II}}$$

(I) Purpose is to measure $(T_2 - T_1)$

$$\text{Adiabatic, const. } V \Rightarrow q_V = 0 \Rightarrow \Delta U_{\text{I}} = 0$$

(II) Purpose is to measure heat q_V needed to take prod. + cal. from T_2 back to T_1 .

$$q_V = \int_{T_2}^{T_1} C_V (\text{Prod.} + \text{Cal.}) dT = \Delta U_{\text{II}}$$

$$\therefore \boxed{\Delta U_{\text{rx}}(T_1) = -\int_{T_1}^{T_2} C_V (\text{Prod.} + \text{Cal.}) dT}$$

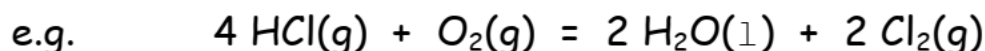
Now use $H = U + pV$ or $\Delta H = \Delta U + \Delta(pV)$

Assume only significant contribution to $\Delta(pV)$ is from gases.

Ideal gas $\Rightarrow \Delta(pV) = R\Delta(nT)$

Isothermal $T = T_1 \Rightarrow \Delta(pV) = RT_1\Delta n_{\text{gas}}$

$$\therefore \boxed{\begin{aligned} \Delta H_{\text{rx}}(T_1) &= \Delta U_{\text{rx}}(T_1) + RT_1\Delta n_{\text{gas}} \\ \Delta H_{\text{rx}}(T_1) &= -\int_{T_1}^{T_2} C_V (\text{Prod.} + \text{Cal.}) dT + RT_1\Delta n_{\text{gas}} \end{aligned}}$$



$$T_1 = 298.15 \text{ K}$$

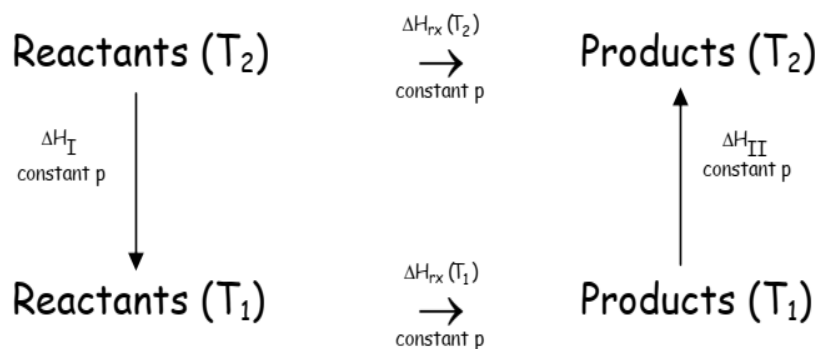
$$\Delta U_{\text{rx}}(T_1) = -195.0 \text{ kJ} \quad \Delta n_{\text{gas}} = -3 \text{ moles}$$

$$\begin{aligned} \Delta H_{\text{rx}}(T_1) &= -195.0 \text{ kJ} + (-3 \text{ mol})(298.15 \text{ K})(8.314 \times 10^{-3} \text{ kJ/K-mol}) \\ &= -202.43 \text{ kJ} \end{aligned}$$

Temperature dependence of ΔH_{rx}

Suppose know ΔH_{rx} at some temperature T_1 (e.g. at 298.15 K) and we want to know it at some other temperature T_2 .

Generally the difference is small... often we assume that there is no temperature dependence if the difference between T_1 and T_2 is "small". If the difference between T_1 and T_2 is large enough, we can calculate $\Delta H_{rx}(T_2)$ from the heat capacities of the reactants and products (assuming no phase change in any component).



$$\Delta H_{rx}(T_2) = \Delta H_I + \Delta H_{rx}(T_1) + \Delta H_{II}$$

$$\Delta H_{rx}(T_2) = \Delta H_{rx}(T_1) + \int_{T_2}^{T_1} C_p(\text{react.}) dT + \int_{T_1}^{T_2} C_p(\text{prod.}) dT$$

$$\Delta H_{rx}(T_2) = \Delta H_{rx}(T_1) + \int_{T_1}^{T_2} [C_p(\text{prod.}) - C_p(\text{react.})] dT$$

$$\Delta H_{rx}(T_2) = \Delta H_{rx}(T_1) + \int_{T_1}^{T_2} \Delta C_p dT$$